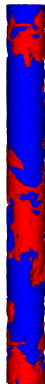
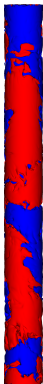


High Rayleigh Number Convection in a Slender Cylinder for Prandtl Number of 1

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Rayleigh-Bénard Convection in cylindrical containers

Previous Results for $Pr \simeq 1$

- Experiments for heat transport at very high Rayleigh number $Nu \propto Ra^\beta$:
 - Brno, Chicago, Eugene, Trieste, Göttingen, Grenoble
 - Range from about $Ra = 10^6 - 10^{15}$, $0.5 < \Gamma < 1$
 - Results for a sharp transition in scaling exponent β are mixed.
- DNS for heat transport at very high Rayleigh number $Nu \propto Ra^\beta$:
 - Stevens, et. al (2011): Highest $Ra = 2 \times 10^{12}$ for $\Gamma = 1/2, 1/4$.
 - No transition in scaling exponent β .

Dimensionless Boussinesq equations

$$\begin{aligned}(\partial_t + \mathbf{u} \cdot \nabla) \mathbf{u} &= -\nabla P + \sqrt{\frac{Pr}{Ra}} \nabla^2 \mathbf{u} + T \hat{\mathbf{z}} \\(\partial_t + \mathbf{u} \cdot \nabla) T &= \frac{1}{\sqrt{Ra Pr}} \nabla^2 T \\ \nabla \cdot \mathbf{u} &= 0\end{aligned}$$

- $\mathbf{u} = (u_x, u_y, u_z)$ = velocity field, T = temperature, P = pressure field
- Ra =Rayleigh number= $(\alpha g H^3 / \kappa \nu) \Delta T$, Pr =Prandtl number= ν / κ
- Γ = diameter/depth for cylinders
- ν =kinematic viscosity, κ =therm diffusivity, α =therm exp coeff, g =gravity
- Variables rescaled with free-fall velocity $U_f = \sqrt{g \alpha (\Delta T) H}$, temperature ΔT , and height H

Fine resolution with Nek5000—Paul Fischer ANL

$$\Gamma = 0.1, Pr = 1$$

Ra	N	N_e	$N_{e,z}$	$N_e N^3$	Runtime (t_f)
1×10^{11}	9	192,000	300	1×10^8	136
1×10^{12}	12	537,600	400	7×10^8	58
1×10^{13}	13	925,200	500	2×10^9	24
1×10^{14}	11	17,145,600	1200	2×10^{10}	14
1×10^{15}	11	17,145,600	1200	2×10^{10}	7

N = polynomial order

N_e = total number of elements

$N_{e,z}$ = number of elements in z direction

Largest runs done on Mira with 524,288 MPI tasks

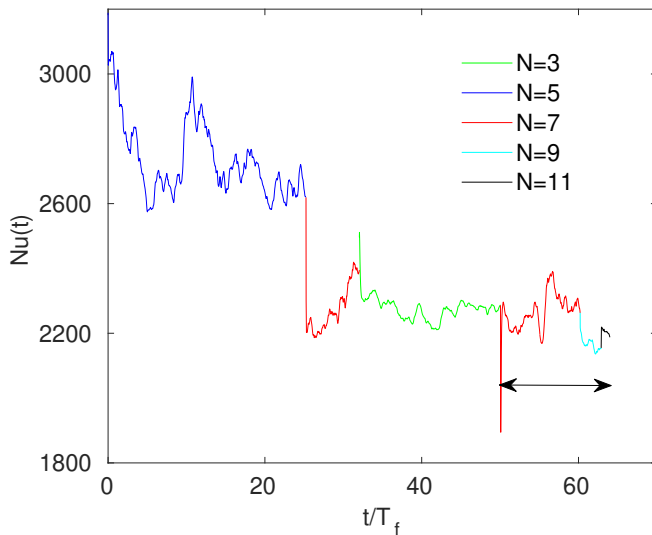
See JS, Emran & Schumacher, New J. Phys. (2013) for more info.



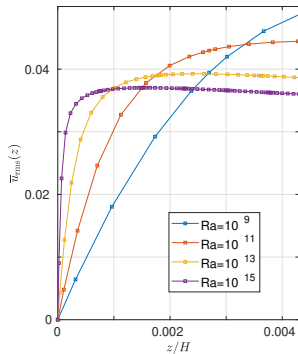
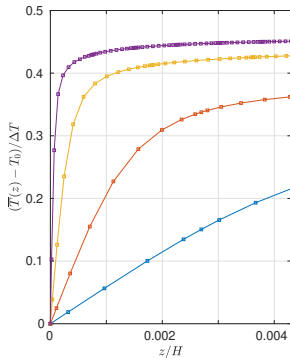
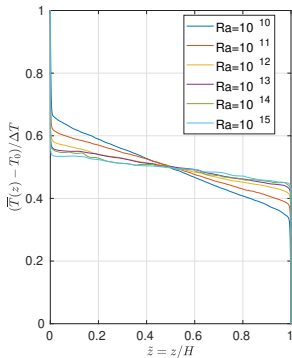
Convergence of Nusselt number

$$Nu = |\langle dT/dz \rangle_{A,t}|/A$$

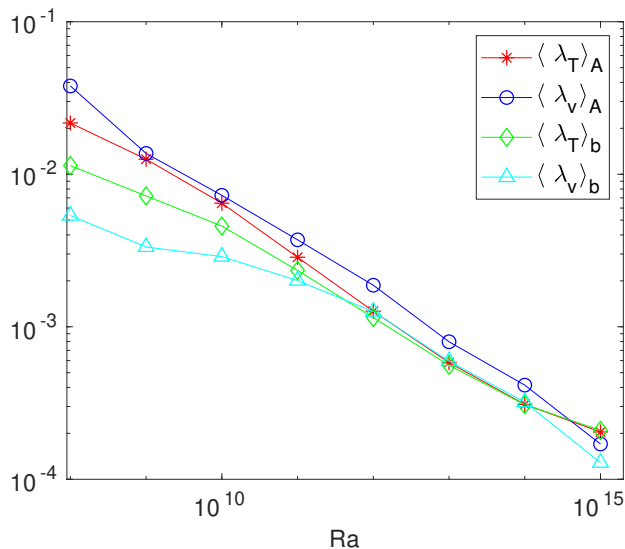
$$Ra = 1 \times 10^{14}$$



Temperature and Velocity profiles



Boundary Layer thicknesses

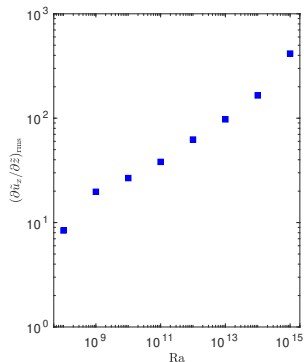
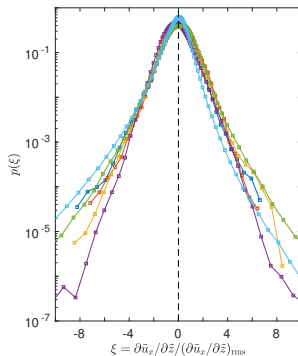
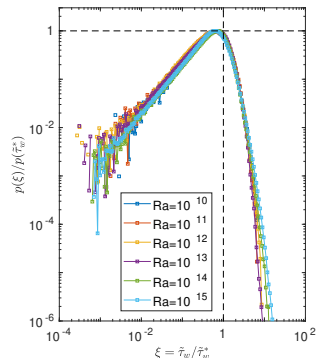


area, $r < 0.05$

bulk, $r < 0.03$

Wall shear stress and velocity gradients

$$\tau_w(x, y, z = 0) = \sqrt{\frac{Pr}{Ra} \left[\left(\frac{\partial u_x}{\partial z} \right)^2 + \left(\frac{\partial u_y}{\partial z} \right)^2 \right]}$$



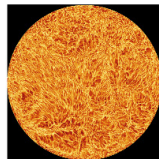
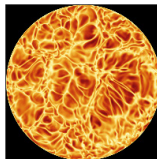
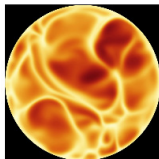
Boundary Layer structure

$$Ra = 1 \times 10^{11}$$

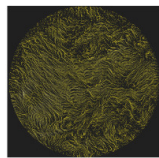
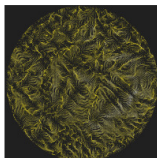
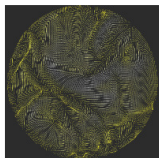
$$Ra = 1 \times 10^{13}$$

$$Ra = 1 \times 10^{15}$$

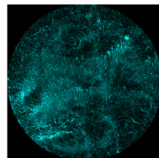
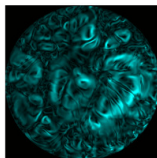
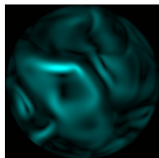
Temp →



Streamlines →



Wall shear
stress →



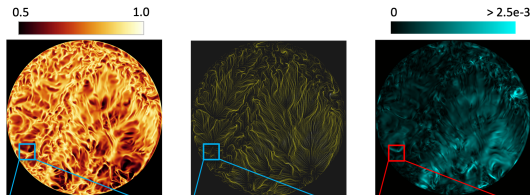
Different Aspect Ratios, $Ra = 1 \times 10^{10}$

Temperature

Streamlines

Wall shear stress

$\Gamma = 1.0$

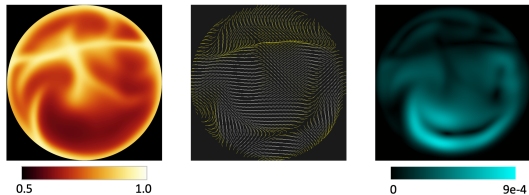


$\Gamma = 1.0$

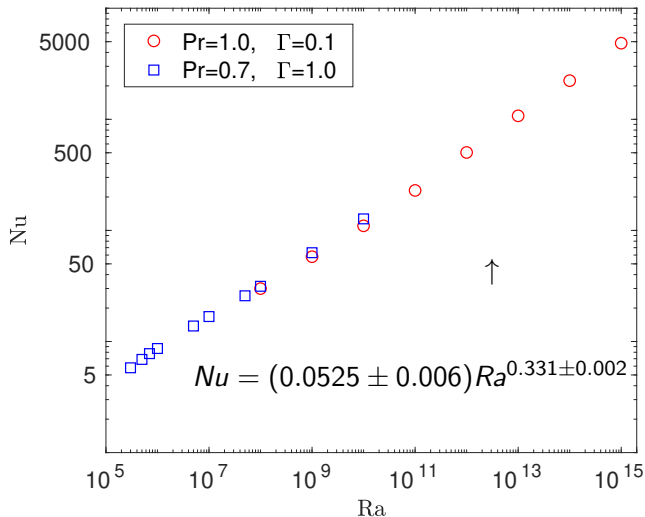
Zoom



$\Gamma = 0.1$

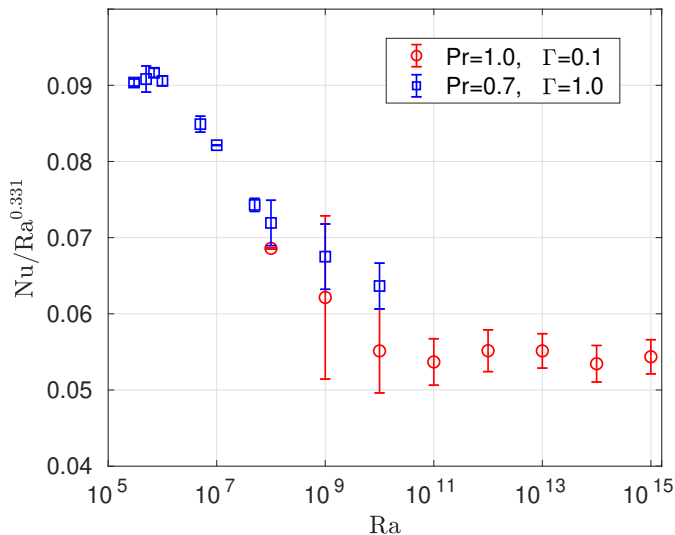


Nusselt Number



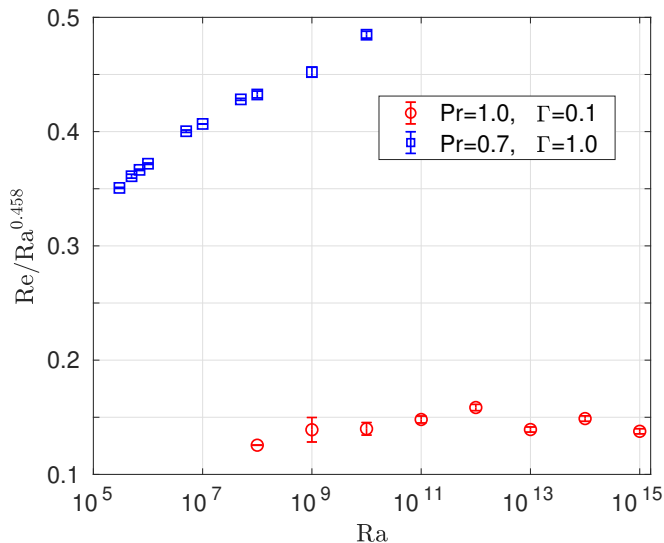
Good agreement w/ Malkus (exponent = 1/3) & Spiegel (prefactor = 0.07)

Nusselt Number, compensated plot



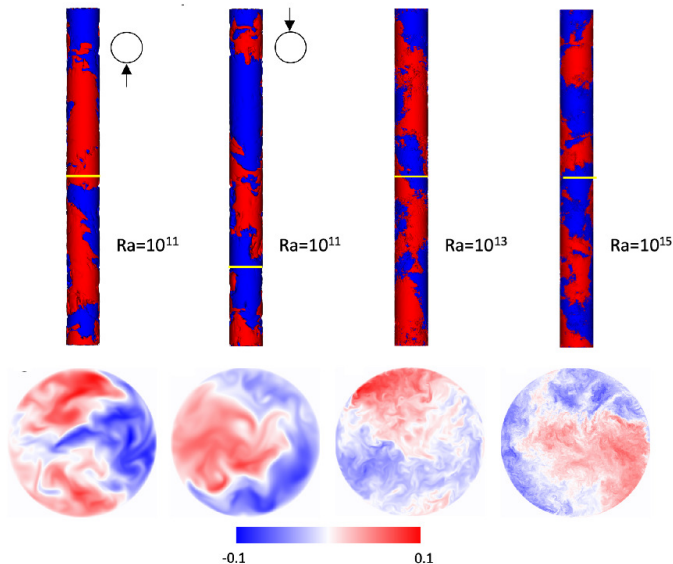
Reynolds Number, compensated plot

$$Re = \langle u_x^2 + u_y^2 + u_z^2 \rangle_{V,t}^{1/2} \left(\frac{Ra}{Pr} \right)^{1/2}$$



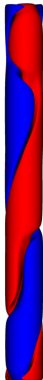
Flow states

$\Gamma = 0.1, Pr = 1$, Plots of u_z

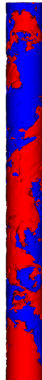


Movies

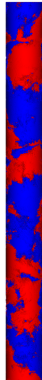
$Pr = 1.0, \Gamma = 0.1$



$Ra = 1 \times 10^8$



$Ra = 1 \times 10^{11}$



$Ra = 1 \times 10^{15}$

Conclusions

- Well resolved, very high Rayleigh number simulations for $\Gamma = 0.1$ and $Pr = 1.0$ have been performed.
- Scaling laws have been determined for heat ($\propto Ra^{0.331}$) and momentum transport ($\propto Ra^{0.458}$) up to $Ra = 10^{15}$.
- Aspect ratio matters for momentum transport, but not for heat transport.
- Heat transport scaling is consistent with the 1/3-power law of Malkus.

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