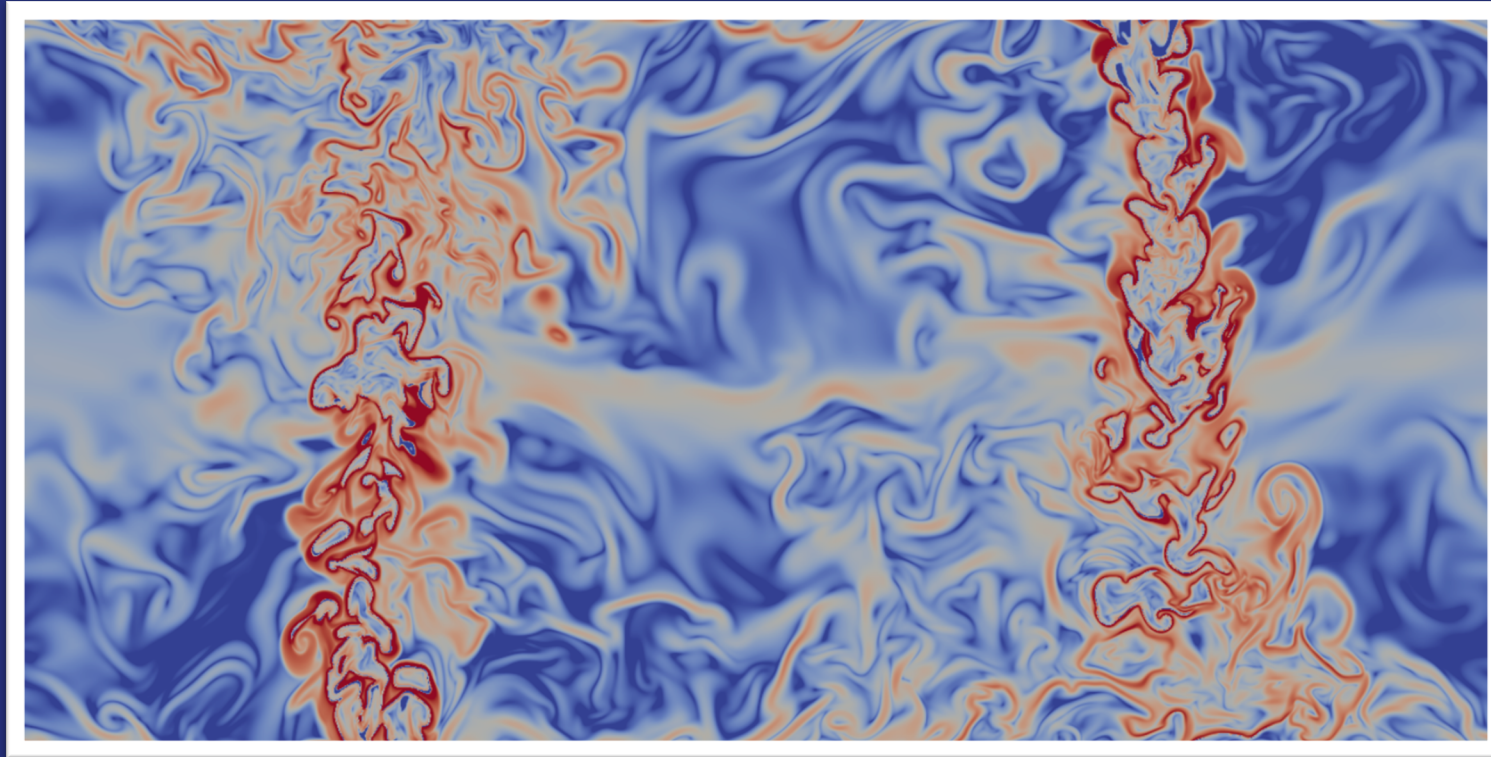


Mixing by plumes in boxes



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Imperial College London

What is the mixing efficiency?

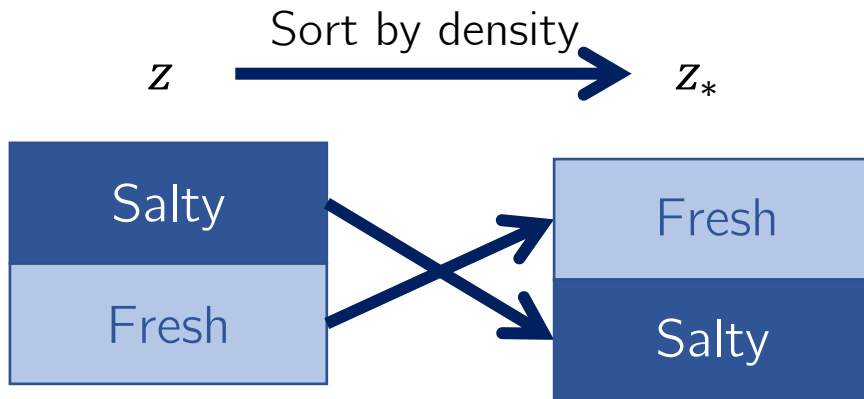
“mixing efficiency... seeks to provide a number quantifying the ability of a particular turbulent mixing event in dissipating [mechanical energy] preferentially diffusively rather than viscously.”

Tailleux, JFM 2009

$$\eta = \frac{\text{Energy used in mixing}}{\text{Energy available for mixing}}$$

Energy used in mixing = increase in BPE

$$E_p = \int_V \rho g z \, dz = \underbrace{\int_V \rho g z_* \, dz}_{\text{Background Potential Energy}} + \underbrace{\int_V \rho g (z - z_*) \, dz}_{\text{Available Potential Energy}}$$



BPE is minimum PE reachable by adiabatic rearrangement of fluid parcels.

Winters, Lombard, Riley & D'Asaro, *J Fluid Mech*, 289 (1995)

Peltier & Caulfield *Ann Rev of Fluid Mech* 35 (2003)

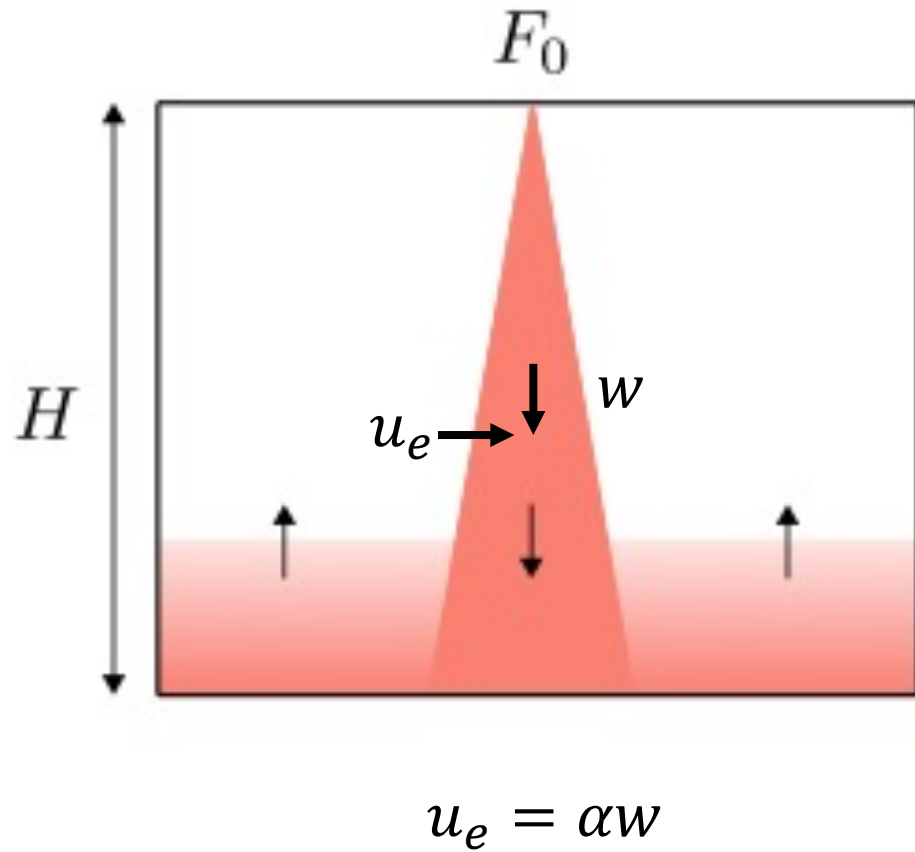
Mixing increases the background potential energy (BPE).

Available potential energy (APE) is present if the system is gravitationally unstable.

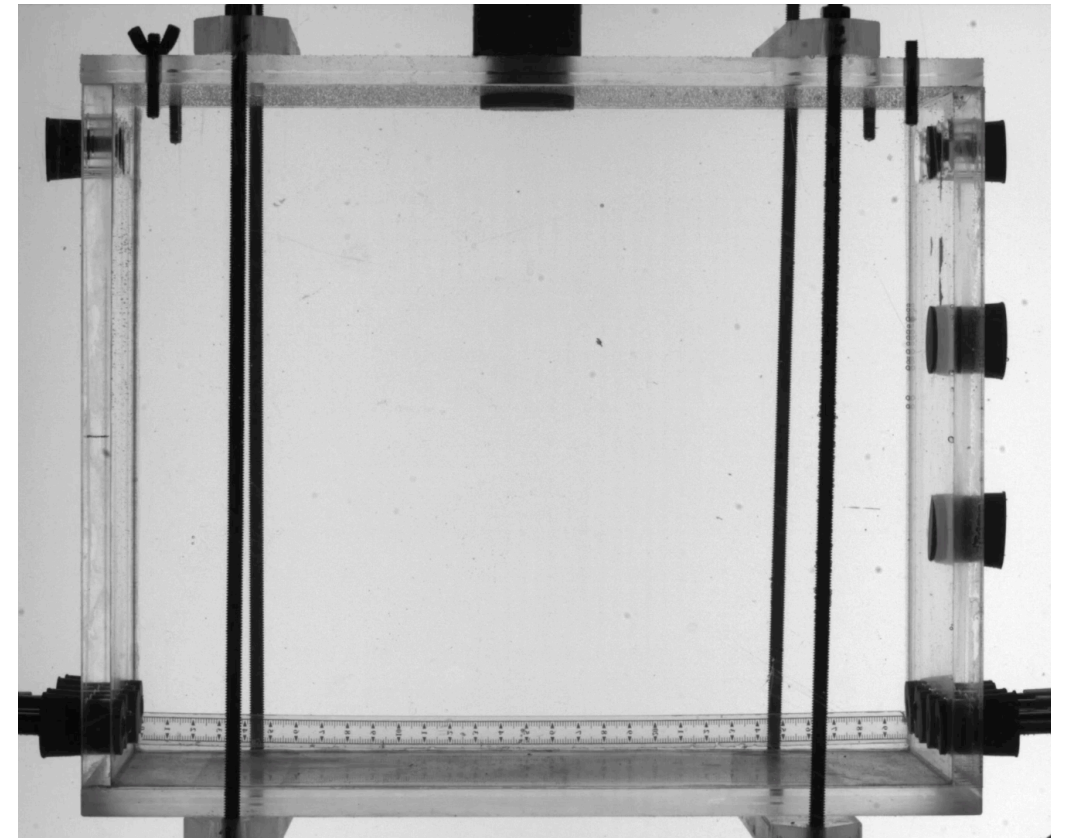
$$\text{Total available energy: } \int_V \left[\underbrace{\rho g(z - z_*)}_{E_a} + \underbrace{\frac{1}{2} \rho v^2}_{E_k} \right] dV$$

$$\eta = \frac{\Delta E_b}{|\Delta E_a + \Delta E_k|}$$

Filling box



Germes (1975) Forced plumes and mixing of liquids in tanks. *J Fluid Mech* 71 (601–623)



Video: Jamie Partridge

Filling box: asymptotic state

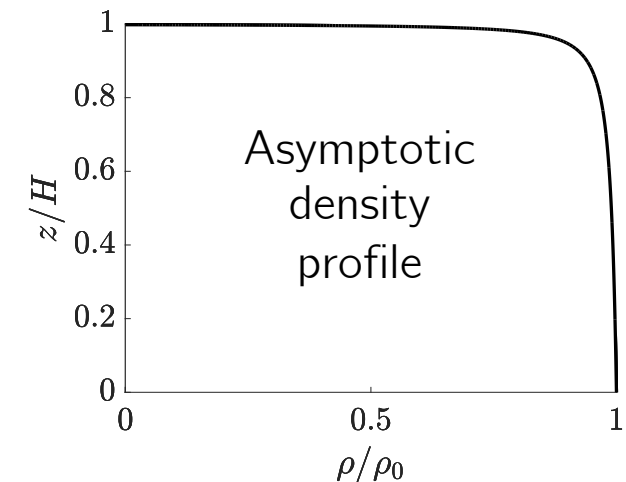
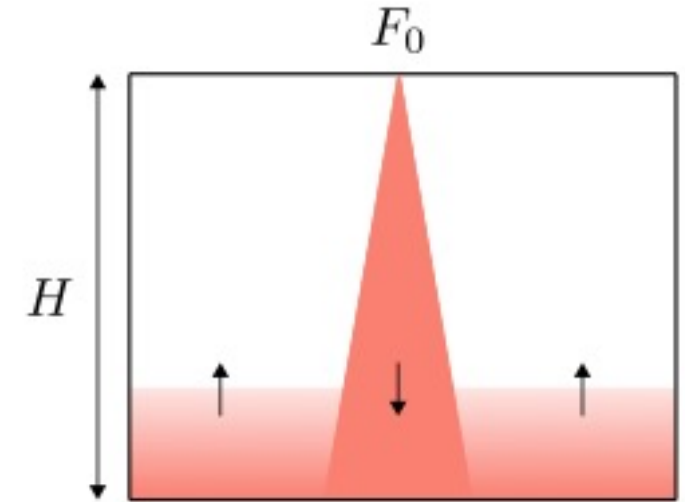
$$\frac{\partial \rho(z, t)}{\partial t} = \frac{\hat{\rho} F_0}{gV}$$

$\hat{\rho}$ = reference density

V = box volume

$$\frac{dE_b}{dt} = g \int_V \frac{\partial \rho}{\partial t} z dV - \hat{\rho} F_0 z_0 = \frac{\hat{\rho} F_0 H}{2}$$

$$\frac{dE_a}{dt} = \hat{\rho} F_0 H \quad \longrightarrow \quad \eta_i = \frac{1}{2}$$



Germeles model

ζ = height m = momentum flux

τ = time q = volume flux

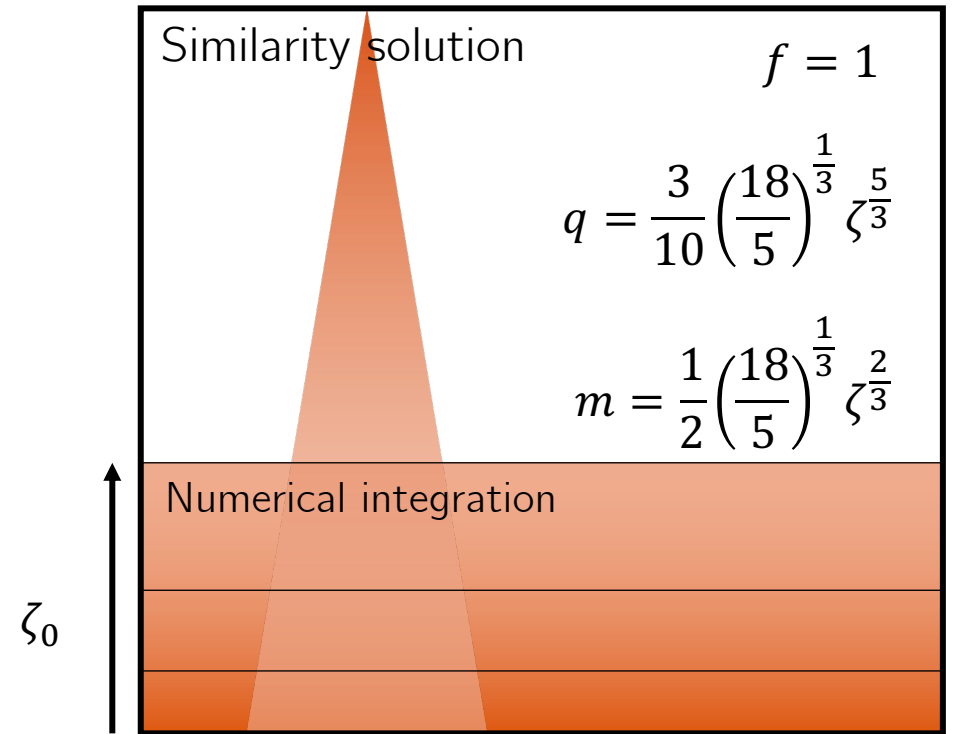
δ = buoyancy f = buoyancy flux

$$\frac{dq}{d\zeta} = m$$

$$\frac{dm^2}{d\zeta} = \frac{qf}{m^2}$$

$$\frac{df}{d\zeta} = q \frac{\partial \delta}{\partial \zeta}$$

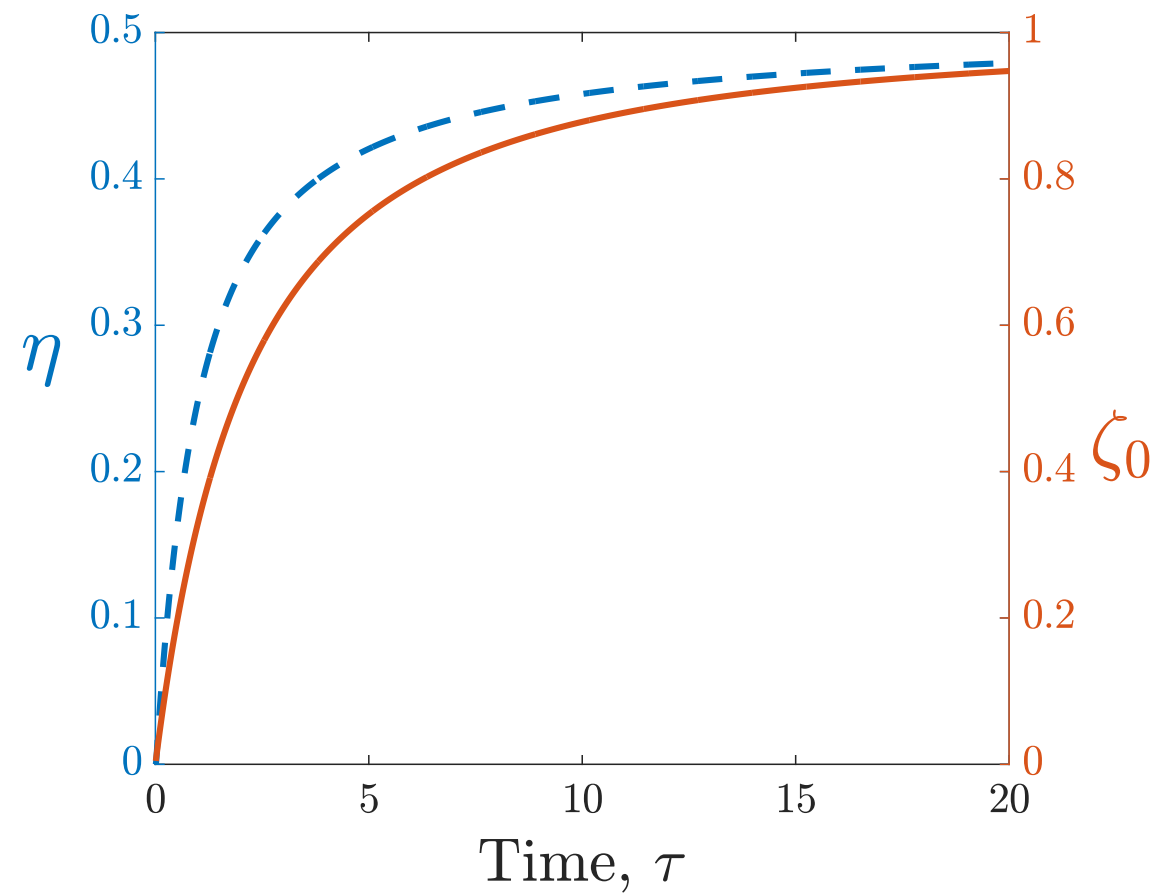
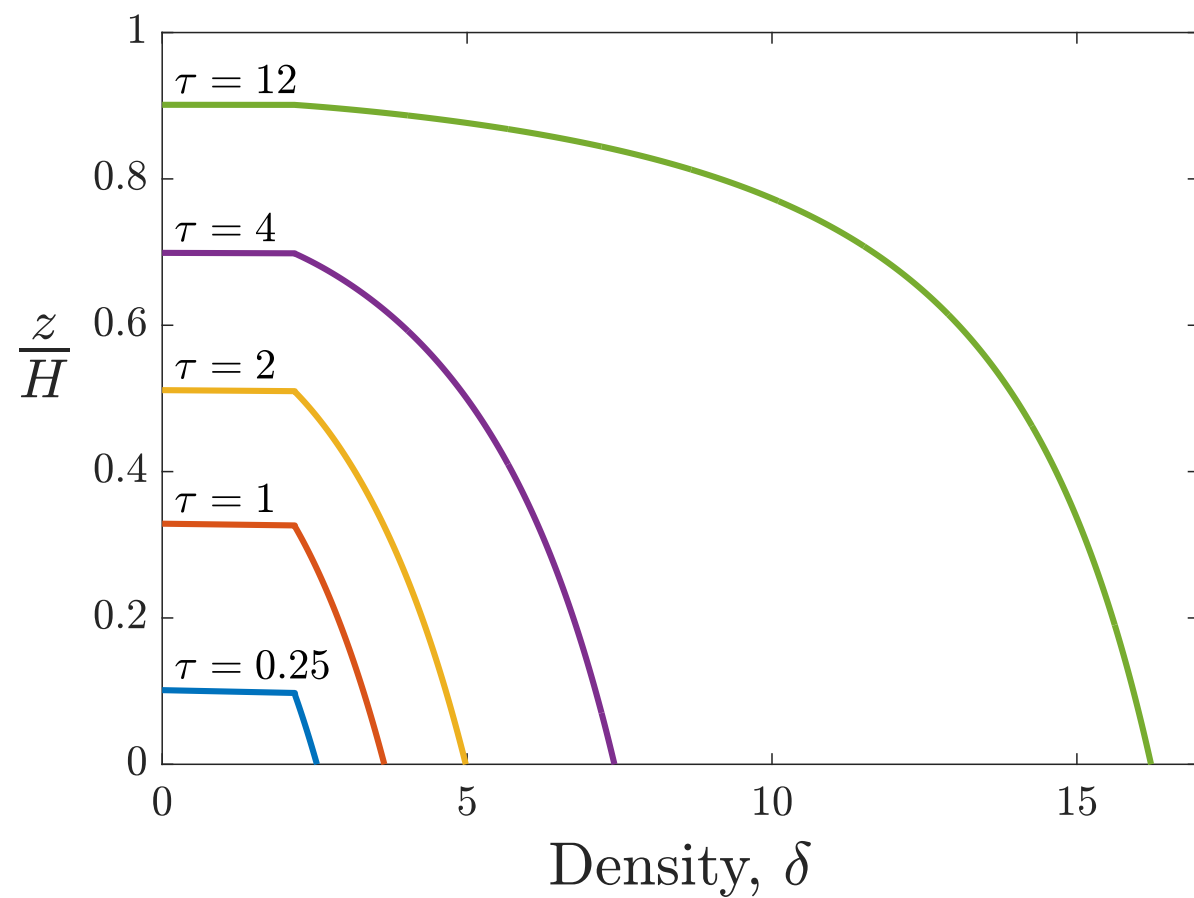
$$\frac{\partial \delta}{\partial \tau} = q \frac{\partial \delta}{\partial \zeta}$$



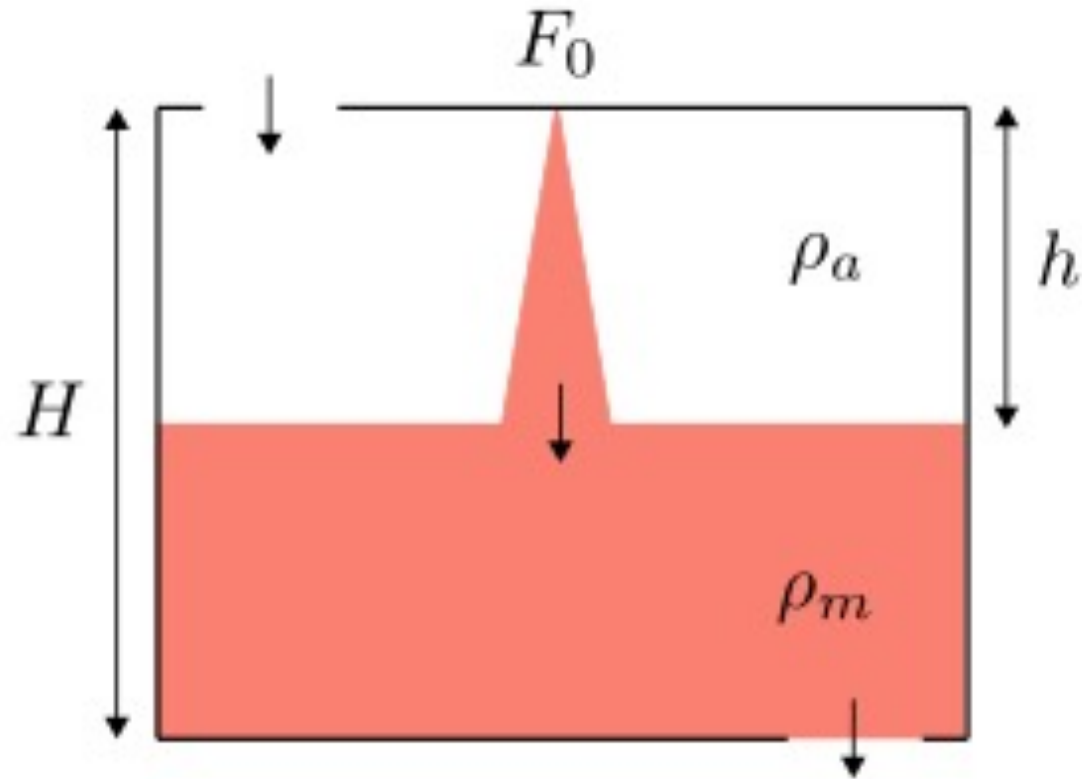
Germeles (1975) Forced plumes and mixing of liquids in tanks. *J Fluid Mech* 71 (601–623)

Worster & Huppert (1983) Time-dependent density profiles in a filling box. *J Fluid Mech* 132 (457–466)

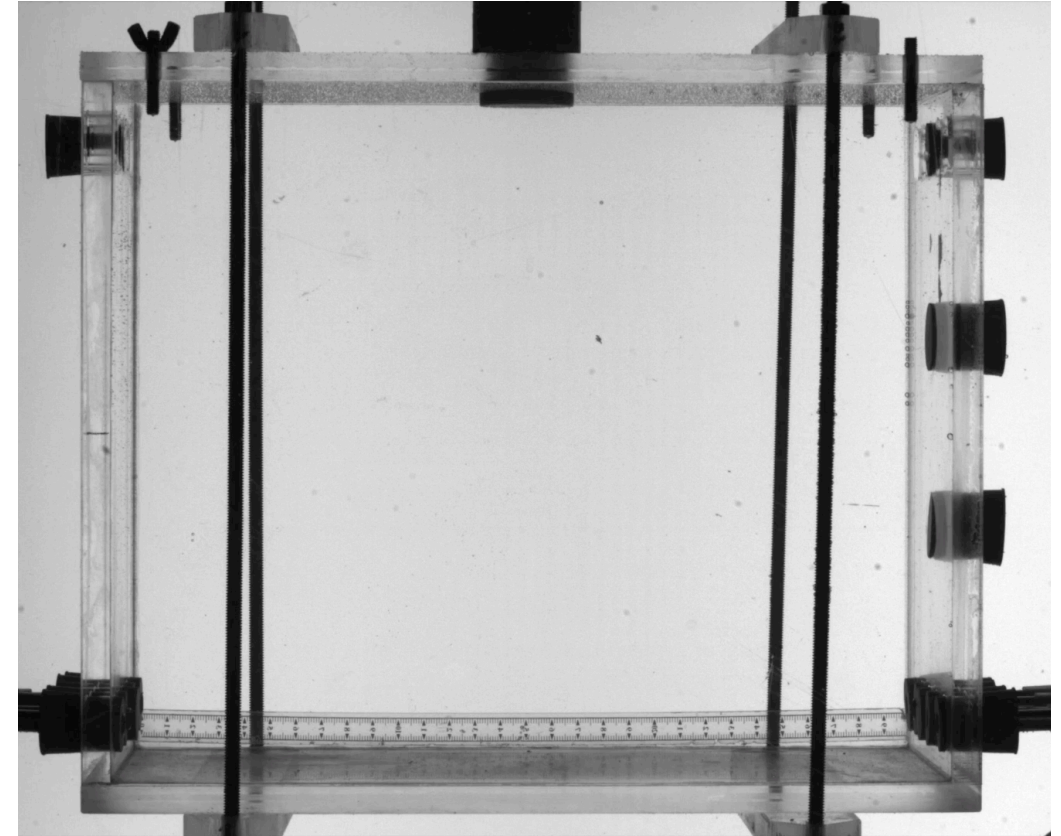
Filling box: transient



Emptying-filling box



Linden, Lane-Serff & Smeed (1990) Emptying filling boxes: the fluid mechanics of natural ventilation. *J Fluid Mech* 212 (309-335)



Video: Jamie Partridge

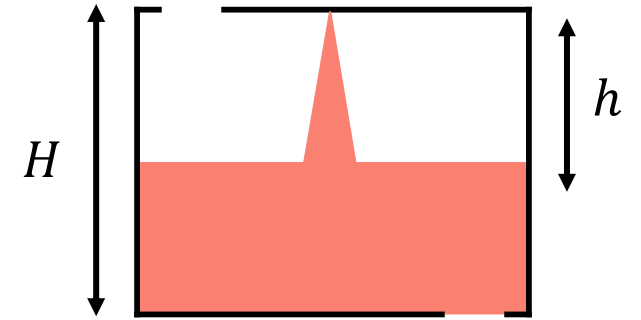
Emptying-filling box: steady state

In steady state: $\left(\frac{\xi}{1-\xi}\right)^{1/2} = \frac{A^*}{C \alpha^2 H^2}$

$$\xi = \frac{h}{H}$$

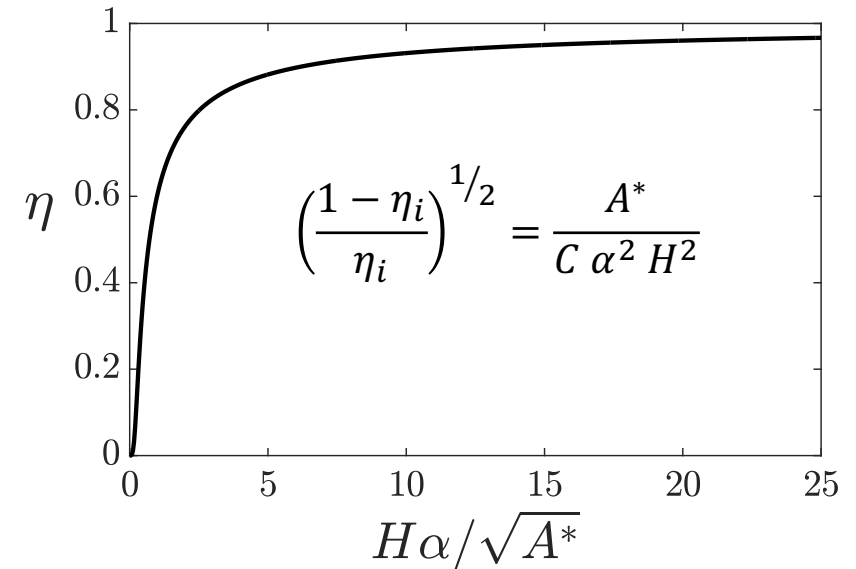
$C = \text{constant}$

$A^* = \text{rescaled opening area}$



$$\frac{dE_b}{dt} = (H - h)\hat{\rho}F_0 \quad \frac{dE_a}{dt} = \hat{\rho}F_0H$$

$$\longrightarrow \eta_i = 1 - \xi$$

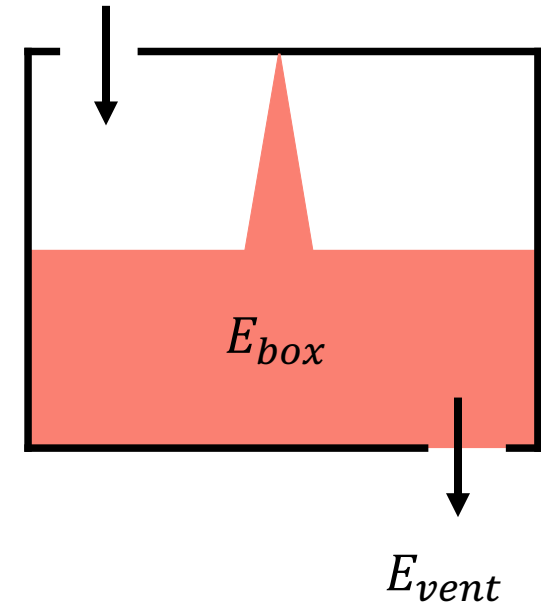


Germeles model with ventilation

$$Q_v = A^* \left(\int_0^H g' dz \right)^{\frac{1}{2}}$$

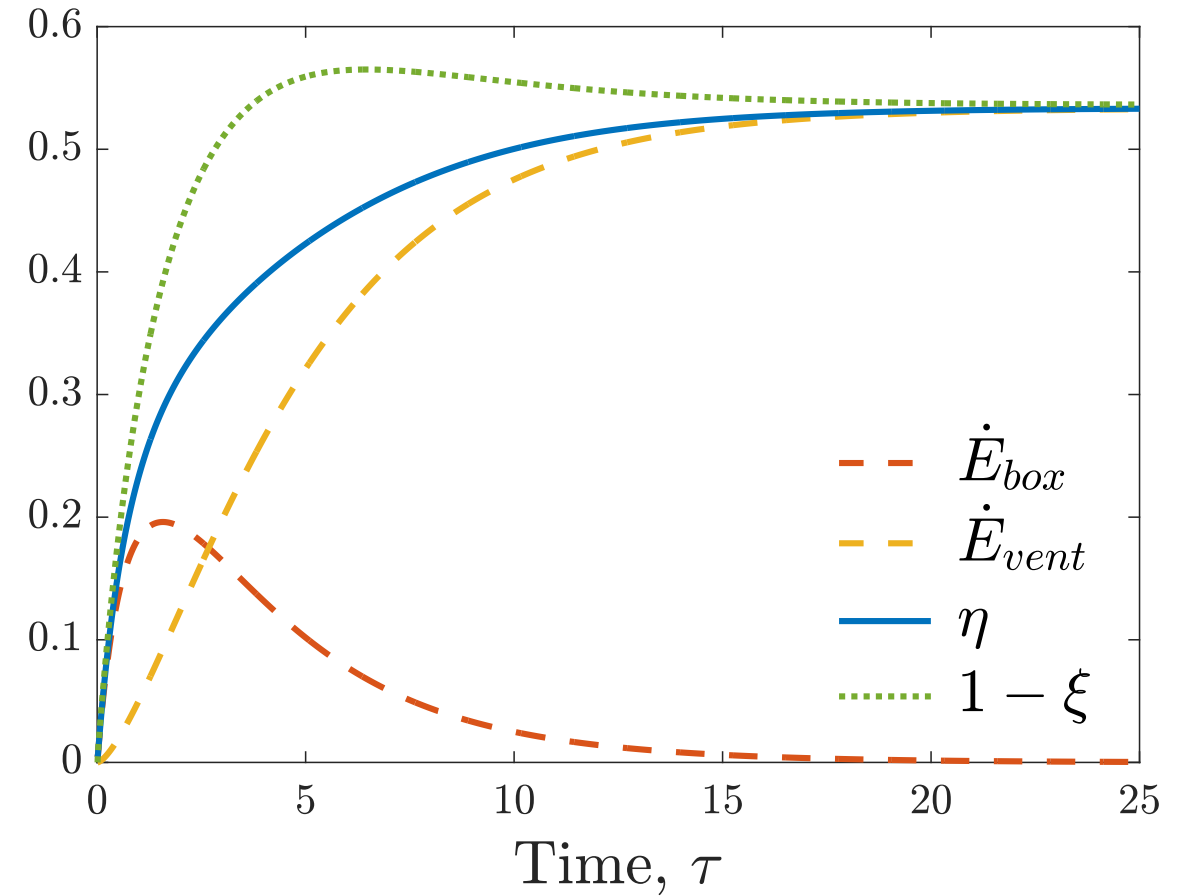
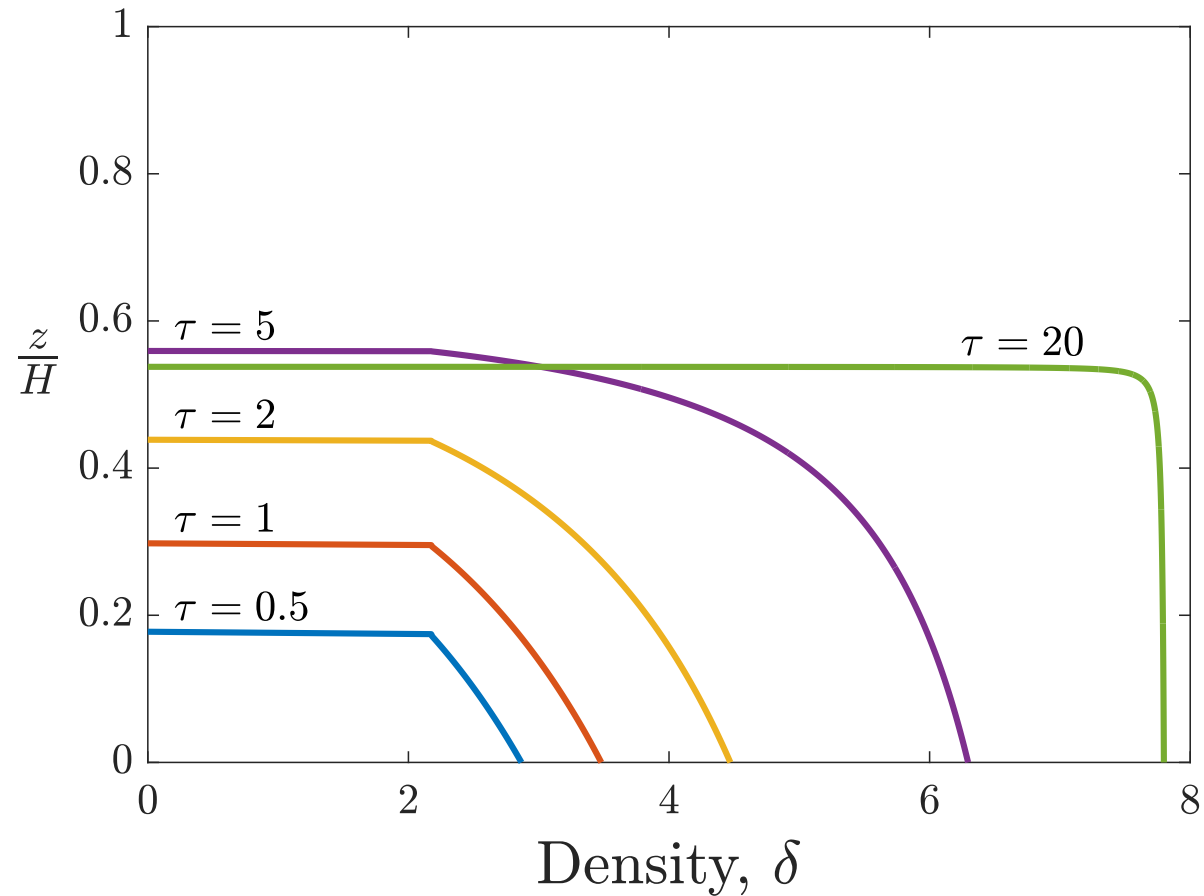
E_{box} = Increase in PE of density profile in box

E_{vent} = PE lost through ventilation



Sandbach & Lane-Serff (2011) Transient buoyancy-driven ventilation:
Part 1. Modelling advection. *Build Environ* 46 (1578–1588)

Emptying-filling box: transient



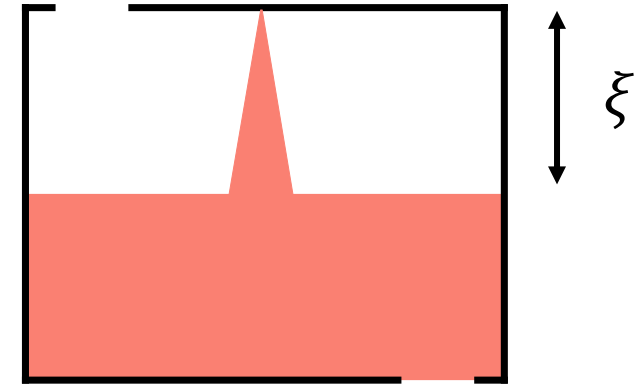
Mixing efficiency of closed vs open systems

Filling box in asymptotic state:

$$\eta_i = \frac{1}{2}$$

Emptying-filling box in steady state:

$$\eta_i = 1 - \xi$$



Davies Wykes, Hogg, Partridge & Hughes (2019) Energetics of mixing for the filling box and the emptying-filling box. *Environ Fluid Mech* **19**, 819–831

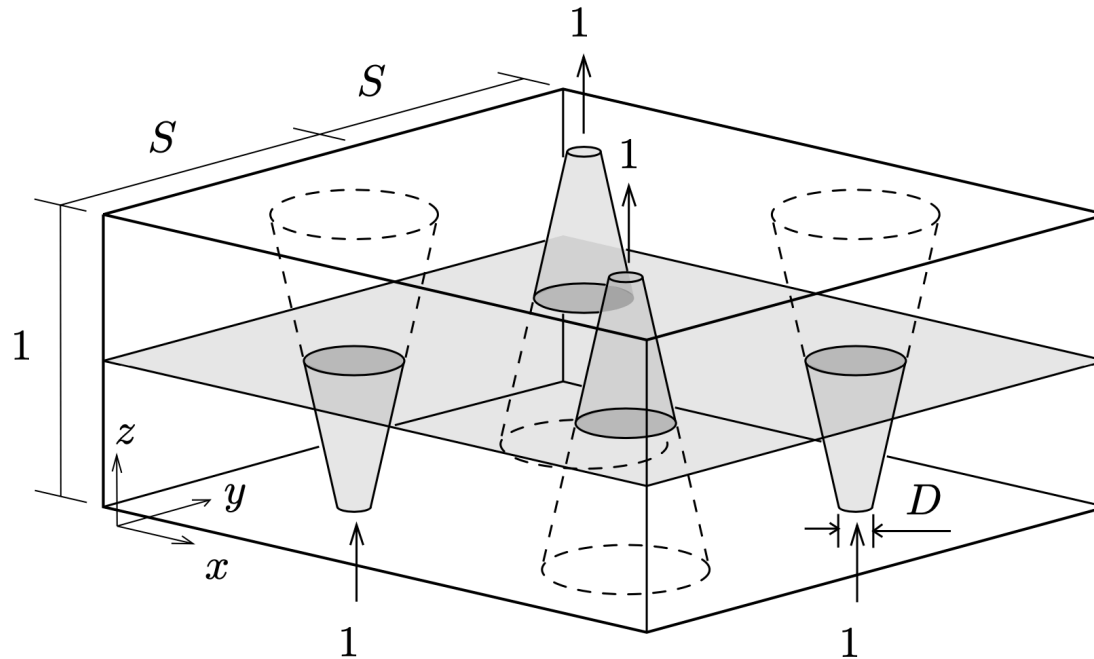
DNS of equal and opposite plumes in a box

$$Pr = 0.7$$

$$Re = 4185$$

$$Ra = 1.24 \times 10^7$$

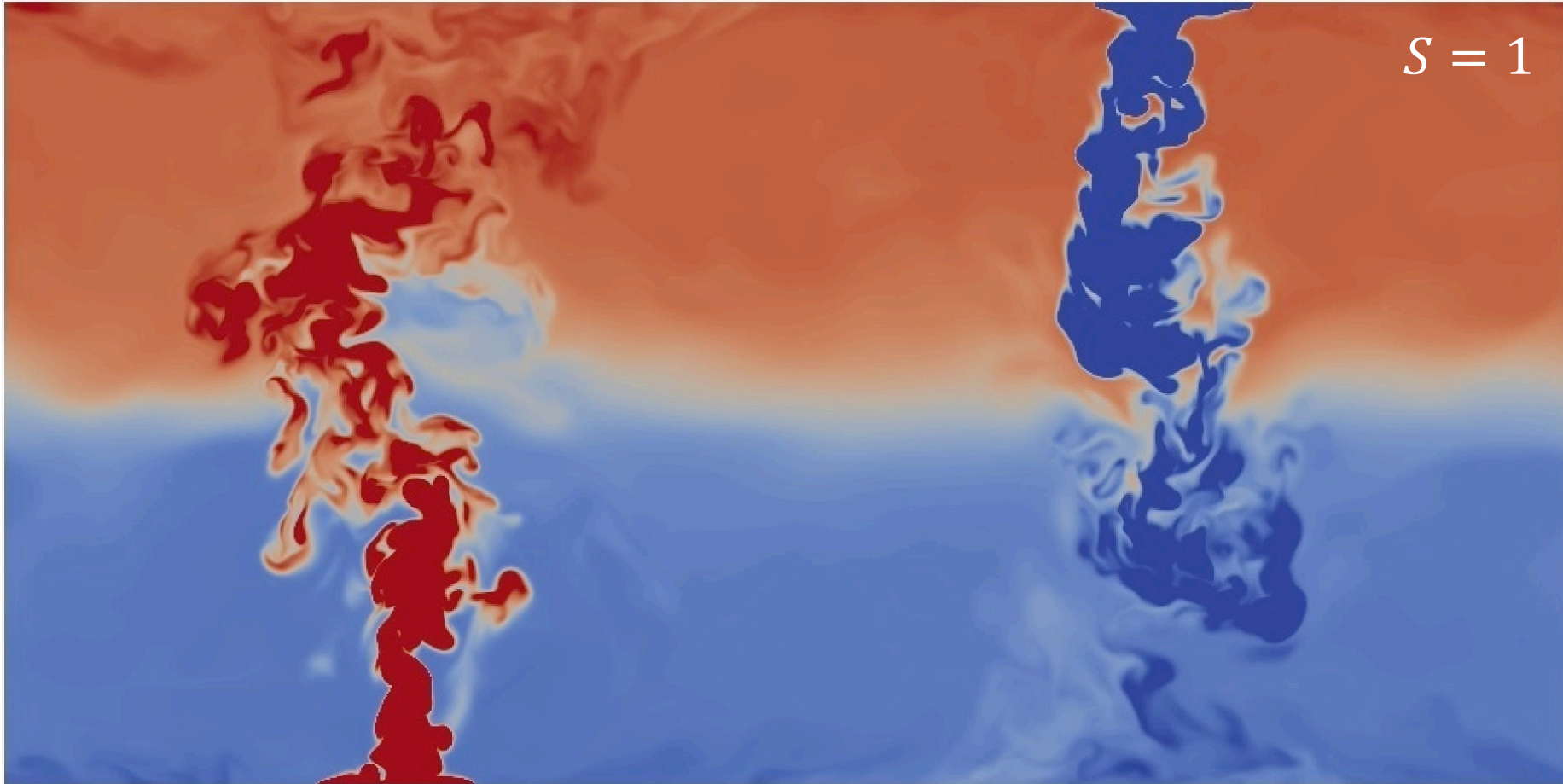
$$D = 1/5$$



S	$Nx \times Ny \times Nz$
1/2	$768 \times 768 \times 768$
7/12	$896 \times 896 \times 768$
2/3	$1024 \times 1024 \times 768$
1	$1536 \times 1536 \times 768$
4/3	$2048 \times 2048 \times 768$

Craske & Davies Wykes (2020). The entrainment and energetics of turbulent plumes in a confined space. *J of Fluid Mech*, **883**, A2

Plumes create a two-layer stratification



Local available potential energy

$$E_a = \int_V b (z_* - z) dz \longrightarrow E_a = b(z_* - z) - \int_0^{z-z_*} b_*(z - \hat{z}, t) d\hat{z} \geq 0$$

$$E_b = -bz - E_a$$

Holliday & McIntyre 1981, JFM

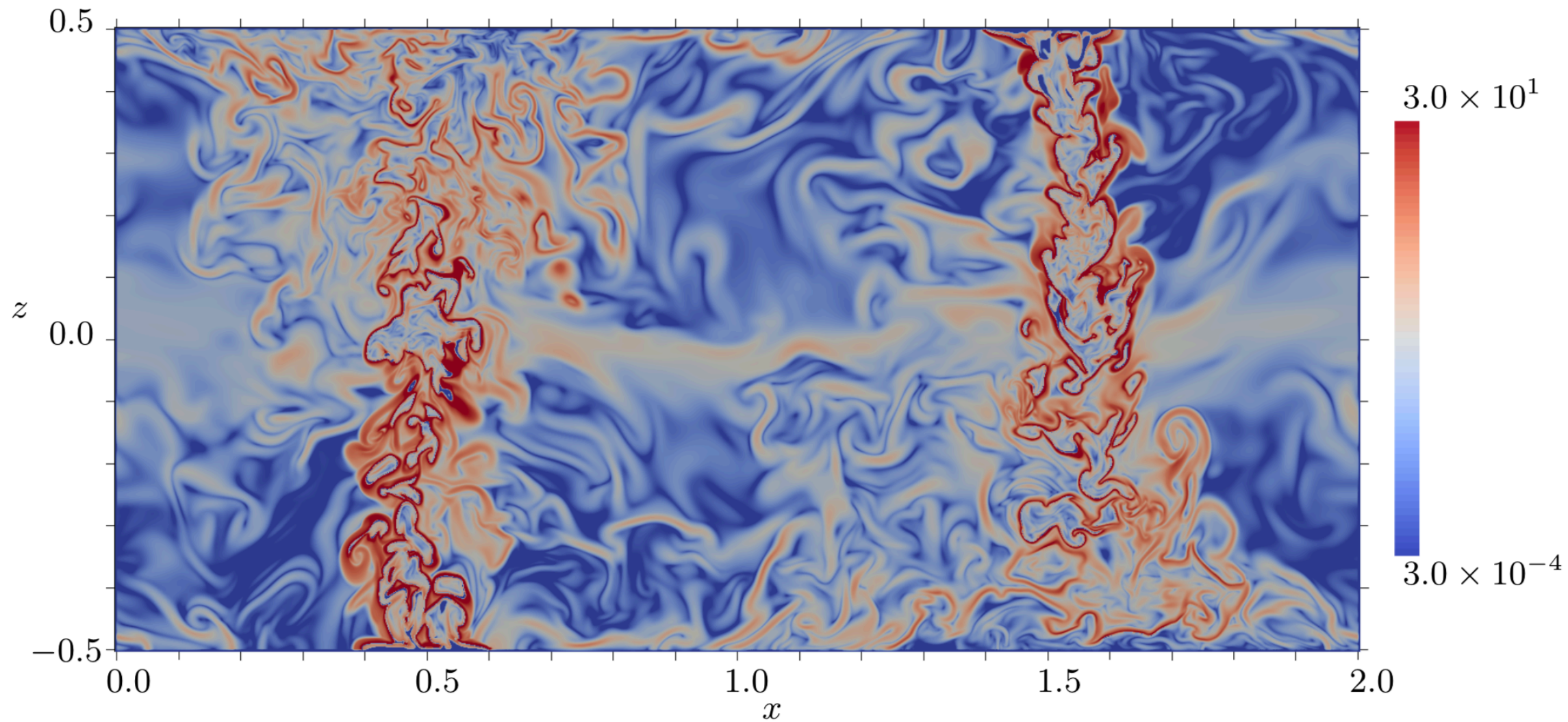
$$\frac{\partial E_k}{\partial t} + \nabla \cdot (\mathbf{u} E_k + \dots) = -\Phi_z - \varepsilon$$

$$\Phi_z = w(b_* - b)$$

$$\frac{\partial E_a}{\partial t} + \nabla \cdot (\mathbf{u} E_a + \dots) = \Phi_z - \Phi_d + \dots$$

$$\frac{\partial E_b}{\partial t} + \nabla \cdot (\mathbf{u} E_b + \dots) = \Phi_d + \dots$$

$$\Phi_d = \frac{(\nabla b)^2}{Pe} \frac{dz_*}{db} \qquad \varepsilon = \frac{(\partial_j u_i)^2}{Re}$$



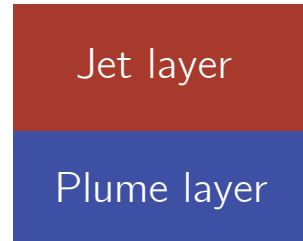
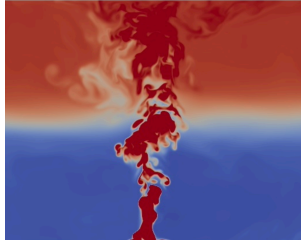
$$\text{BPE Production, } \Phi_d = \frac{(\nabla b)^2}{Pe} \frac{dz_*}{db}$$



Dissipation, ε

BPE Production,
 $\Phi_d > 3$

Energetics within the layers



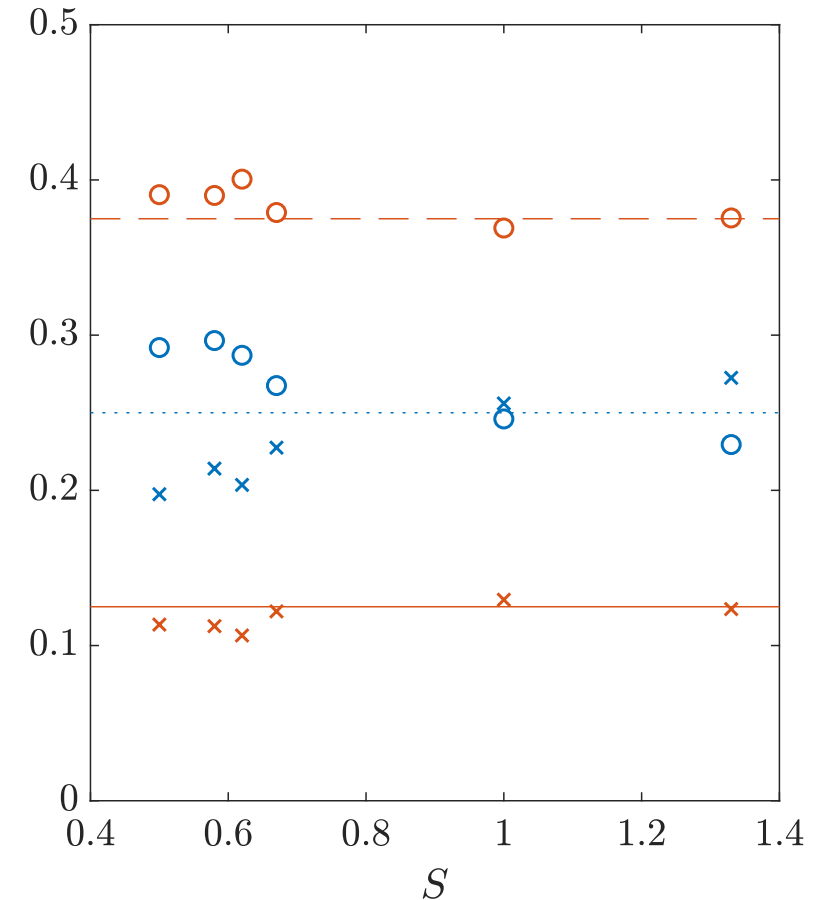
- × Jet layer KE dissipation

$$\langle wE_k \rangle = \frac{\gamma M_m^2}{2Q_m} = \frac{3\gamma}{8}\zeta = \frac{1}{4}$$
- Plume layer KE dissipation

$$\left(1 - \frac{3\gamma}{8}\right)\zeta = \frac{1}{4}$$
- × Jet layer BPE Production

$$\langle wE_a \rangle = (1 - \zeta) \frac{\langle |\Phi_z| \rangle}{2} \Big|_{z=0} = \frac{1}{8}$$
- Plume layer BPE Production

$$1 - \zeta - (1 - \zeta) \frac{\langle |\Phi_z| \rangle}{2} \Big|_{z=0} = \frac{3}{8}$$



Conclusions

- Mixing efficiency in a closed system can be limited when in an open system it is not.
- Energetics are independent of entrainment, even though entrainment determines the buoyancy profile and volume flux.

Davies Wykes, Hogg, Partridge & Hughes (2019)
Energetics of mixing for the filling box and the
emptying-filling box. *Environ Fluid Mech*, **19**, 819–831

Craske & Davies Wykes (2020) The entrainment and
energetics of turbulent plumes in a confined space.
J of Fluid Mech, **883**, A2

